

# CO, NO, and H<sub>2</sub> Adsorption on Ceria-Supported Pd

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We have examined the adsorption of CO, NO, and H<sub>2</sub> on model Pd/ceria catalysts, formed by vapor deposition of Pd metal onto a flat, polycrystalline ceria support, using temperature programmed desorption. For CO adsorption on freshly deposited Pd films, a substantial fraction of the CO reacts to CO<sub>2</sub> in TPD, between 450 and 550 K, indicating that oxygen from ceria can react with CO on Pd. Prereduction of the catalyst by heating in CO or H<sub>2</sub> results in TPD curves which are virtually identical to that observed for Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001), suggesting that electronic interactions between ceria and Pd have a negligible effect on the adsorption properties. For NO, there are differences between Pd/ceria and Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001). A significantly higher fraction of the NO on Pd/ceria reacts to N<sub>2</sub> and N<sub>2</sub>O, and prereduction of the Pd/ceria increases the amount of NO that can adsorb. Both of these results are interpreted as indicating that NO can adsorb on reduced ceria sites which are formed when lattice oxygen at the Pd-ceria interface is transferred to the Pd. For H<sub>2</sub>, the desorption curves are similar to that observed on Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001), except that the low-temperature feature assigned to the bulk hydride is less well resolved. If water is formed upon H<sub>2</sub> adsorption, it apparently readsorbs on the ceria. The implications of these results for reactions involving NO and CO on Pd/ceria are discussed. © 1996 Academic Press, Inc.

## INTRODUCTION

Ceria-supported group VIII metals have received considerable attention in recent years, mainly due to their applications in automotive emissions-control catalysis. Ceria is added to automotive catalysts primarily for its oxygen-storage properties, which result from this oxide's ability to cycle between CeO<sub>2</sub> and CeO<sub>2-x</sub>. However, many questions remain about the nature of interactions between ceria and catalytic metals and there are indications that Pt, Rh, and Pd do not all interact in the same manner with ceria. For example, in at least one catalyst formulation reported in the patent literature (1), it appears that an attempt was made to limit contact between Rh and ceria and maintain contact between Pt and ceria. Furthermore, Rh forms stable perovskites, while Pt and Pd do not (2). Differences were also reported from our laboratory on the oxygen transfer between ceria and supported Pt and Rh (3, 4), although more recent results have shown that this difference could have been due to the ceria structure (5).

In order to address the issue of possible differences between ceria-supported Pt, Rh, and Pd, we compare here the adsorption properties for CO, NO, and H<sub>2</sub> on ceria-supported Pd, Rh, and Pt using a series of model catalysts prepared under UHV conditions. Previous studies have demonstrated that adsorption properties on model catalysts of this type can be related to catalytic rates measured under steady-state conditions. For example, changes with particle size in the desorption kinetics of NO from Rh on model catalysts (6) can be related to changes in the steady-state NO reduction rates observed on high-surface-area catalysts (7). Similarly, changes in desorption kinetics of CO from Pt with particle size could be related to observations of steady-state CO oxidation rates (8, 9). Finally, TPD studies of model Rh-ceria catalysts, prepared using similar conditions to those in the present study, exhibited a ceria-mediated CO oxidation process (3, 10) which is also observable on high-surface-area catalysts (11).

Our present results demonstrate that CO adsorbed on Pd can react with oxygen from the ceria framework to form CO<sub>2</sub> in the same manner reported for Rh on ceria. With this exception, the desorption features for CO are otherwise very similar to that found for Pd on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) (12), suggesting that the Pd itself is not strongly affected. For NO, we observe significantly more dissociation than was found for Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001). Also, for reduced ceria, some of the NO adsorbs and dissociates on the ceria itself, as demonstrated by the significant increase in the adsorption uptakes. The implications of these results in automotive catalysts will be discussed.

## EXPERIMENTAL PROCEDURE

Since the pretreatment and preparation conditions used for ceria can strongly affect the final properties (5), all of the experiments were performed on the same substrate. This substrate was prepared by spray pyrolysis of a 0.3-N aqueous solution of Ce(NO<sub>3</sub>)<sub>3</sub> (99.5% purity, Johnson Matthey) on an  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) single crystal, using an N<sub>2</sub> carrier gas, while holding the sapphire crystal at ~650 K. After ceria deposition, the sample was placed in an oven and held at ~900 K, in air for 2 hr. This procedure was repeated three times to produce a final ceria film ~20  $\mu$ m

thick. Finally, the sample was heated overnight at 970 K, a temperature at least 250 K higher than the decomposition temperature of Ce(NO<sub>3</sub>)<sub>3</sub> (13).

A complete description of the films is given elsewhere (5). Briefly, X-ray diffraction patterns of films prepared using the same procedure demonstrated that the sample had the CeO<sub>2</sub> fluorite structure. Using Scherrer's formula for the line-broadening of the peak at 28.4°, we estimated the ceria crystallite size to be ~9–12 nm. Scanning electron micrographs showed that the films were relatively flat, with cracks or fissures separating irregularly shaped islands of ~1 μm in size. The surface area was found from BET measurements to be 12 m<sup>2</sup>/g. If one assumes that the ceria consists of dense, spherical particles, this surface area would be obtained for particles 0.1 μm in diameter, which implies there must be some porosity in the islands.

The UHV chamber used for the TPD measurements has a base pressure of ~4 × 10<sup>-10</sup> Torr. It is equipped with a cylindrical mirror analyzer for Auger electron spectroscopy (AES) and a quadrupole mass spectrometer, interfaced with a computer for data acquisition and multiplexing. To improve sensitivity and baselines of the TPD, the quadrupole was placed inside a stainless-steel cone with an aperture, in front of which the sample could be placed. The oxide substrate was mounted on a Ta foil that could be cooled to 120 K or heated resistively to 900 K. A chromel-alumel thermocouple, attached to the back side of the α-Al<sub>2</sub>O<sub>3</sub> crystal via a ceramic adhesive, was used to monitor the temperature. The adsorbates were introduced to the chamber through two beam dosers in order to maintain a low base pressure. The pressure in front of the doser has been estimated to be approximately 20 times higher than the background pressure, and exposures quoted in this manuscript were determined using this factor.

The ceria substrate was cleaned by ion bombardment at 500 K to remove all impurities observable by AES, followed by annealing in 1 × 10<sup>-7</sup> Torr O<sub>2</sub> at 900 K for 30 min. The final oxidation-step involved cooling the sample to 400 K in 1 × 10<sup>-7</sup> Torr O<sub>2</sub>. Following evacuation, the noble metals were deposited at room temperature. The model catalysts at this stage will be referred to as "fresh." The AES peak intensities for Pd as a function of metal coverage were very similar to those reported for Pd/α-Al<sub>2</sub>O<sub>3</sub>(0001), suggesting that the growth of the metal film was nearly two-dimensional (12). Simply heating the samples above 650 K resulted in an irreversible, decreased peak intensity for Pd in AES, along with an increased intensity for oxygen, indicating that the metal film coalesced into particles at this temperature. Heating the samples in 1 × 10<sup>-7</sup> Torr CO or H<sub>2</sub> for 10 min at 650 K, followed by briefly heating to 800 K in vacuum, induced changes in the desorption curves. Samples pretreated in this manner will be referred to as "reduced." For most of the experiments in this study, CO was used as the reductant.

For CO and <sup>15</sup>NO, adsorption was performed at room temperature, while H<sub>2</sub> was adsorbed at 120 K. Typical exposures were approximately 10 L (1 Langmuir = 10<sup>-6</sup> Torr · sec = 3.7 × 10<sup>14</sup> molecules/cm<sup>2</sup> for NO at 300 K), which were sufficient to achieve saturation. For all TPD measurements, the heating rate was 10 K/sec. After each NO TPD, oxygen resulting from dissociation was removed by exposing the sample to CO and heating to 700 K. The desorption rates, *r<sub>d</sub>*, in each figure are in arbitrary units, but all curves are drawn to the same scale.

## RESULTS

### CO Adsorption on Pd/CeO<sub>2</sub>

The TPD curve following a saturation exposure of the as-deposited, fresh, 5 × 10<sup>15</sup> Pd/cm<sup>2</sup> film to CO is shown in Fig. 1a. It is very similar to curves obtained from Pd particles on α-Al<sub>2</sub>O<sub>3</sub>(0001) (12), with the exception that a significant amount, ~20%, of the CO reacts to CO<sub>2</sub> between 450 and 550 K. The CO peak exhibits a single maximum at 490 K and a low-temperature shoulder at ~370 K, similar to what is observed for CO from Pd single crystals (14). These desorption features have previously been assigned to CO which is bridge bonded and terminally bonded, respectively (15). The source of the oxygen needed to form CO<sub>2</sub> appears to be the ceria. The Pd was not exposed to

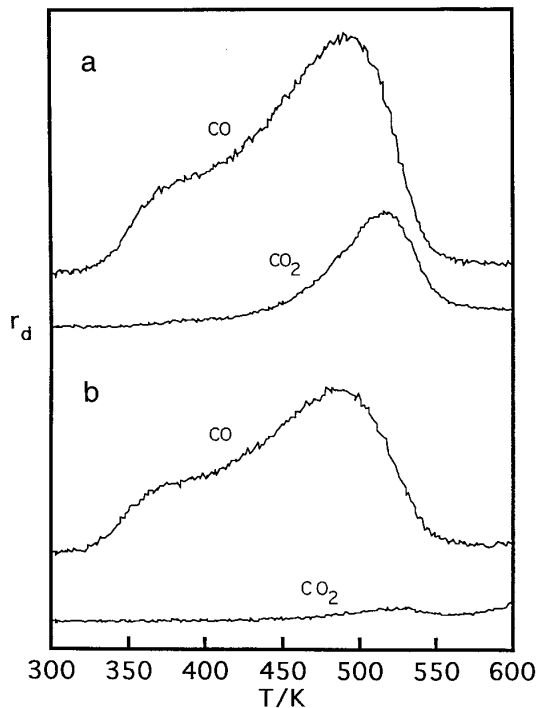


FIG. 1. Saturation TPD curves following CO adsorption at room temperature on a film of 5 × 10<sup>15</sup> Pd/cm<sup>2</sup> (a) as deposited on ceria (fresh) and (b) after mild reduction in CO (reduced).

oxygen prior to the adsorption of CO; furthermore, if the CO<sub>2</sub> was the product of coadsorbed oxygen, it would appear in a peak centered at a lower temperature (16). We found no evidence for carbon deposition from either AES or subsequent TPD curves; therefore, the oxygen is not the result of CO dissociation. Rather, the results for Pd/ceria are very similar to those reported for Rh/ceria (3), where reduction of the ceria is the source of the oxygen.

After heating the film to 700 K during this first TPD measurement, the Pd film coalesced into larger particles, as shown by AES. Subsequent TPD curves for CO were very similar to that shown in Fig. 1a. Except that the amount of CO<sub>2</sub> decreased monotonically, similar to what has been reported for Rh/ceria (3). After the film had coalesced into particles, the sum of the CO and CO<sub>2</sub> peaks remained approximately constant, indicating that the size of the particles did not change substantially following the first annealing cycle. Using the sum of the CO and CO<sub>2</sub> areas in TPD to determine the dispersion and to calculate a particle size, as described elsewhere (17), we estimate the average Pd particle diameter to be  $\sim 9$  nm. The CO TPD curve on the reduced sample, obtained after heating it in CO at 650 K, is shown in Fig. 1b. There is no significant change in the desorption features for CO, but the amount of CO<sub>2</sub> formed is now negligible. Annealing to 950 K in vacuum restored some of the ability of the surface to oxidize CO, as reported previously for Rh/ceria (3), indicating that oxygen could be brought out from the bulk of the ceria.

In order to investigate the effect of Pd particle size, the same adsorption measurements were performed on a film with  $1 \times 10^{15}$  Pd/cm<sup>2</sup>. The TPD curves are not shown because they are so similar to those obtained for  $5 \times 10^{15}$  Pd/cm<sup>2</sup>. The minor differences were as follows: First, the fraction of the CO which reacted to CO<sub>2</sub> in TPD was higher and CO<sub>2</sub> formation appeared to start at slightly lower temperatures. For example, the first TPD curve on the fresh film gave a CO<sub>2</sub> peak area which was 30% of the CO peak area. The increased fraction of CO reacting to CO<sub>2</sub> is consistent with oxygen originating at the edge of the metal crystallites, as suggested in recent reaction measurements (18). Second, the particle size determined after annealing this sample to 700 K, again determined by CO adsorption capacity, was found to be 5.2 nm, which is smaller than that obtained for larger metal coverages and consistent with that found for similar metal coverages on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) (12). There is no evidence for CO adsorption on either oxidized or reduced ceria. Finally, a higher fraction of the CO on the reduced sample desorbed in the 370 K peak for the lower Pd coverage, consistent with the smaller Pd particle size.

#### NO Adsorption on Pd/CeO<sub>2</sub>

In order to examine the role of ceria in the adsorption and dissociation of NO on Pd, we compare the TPD curves for Pd/ceria with those for Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) (12). Since

the TPD curves for NO on Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) were virtually identical to those obtained for Pd on amorphous silica (19), we suggest that the sapphire support is noninteracting and that the results on this surface simply represent the desorption of NO on small Pd particles. Figures 2 and 3 show the desorption results for NO from the fresh and reduced Pd films of 5 and  $1 \times 10^{15}$  Pd/cm<sup>2</sup>, respectively, with the analogous results for the same metal coverages on the sapphire crystal in the upper right corner. The results on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) were obtained after heating the films to 700 K to form particles. To remove oxygen formed by NO dissociation, CO was adsorbed and the sample flashed to 700 K between NO TPD measurements. <sup>15</sup>N was used in all of the experiments to eliminate any ambiguity in determining the products.

For  $5 \times 10^{15}$  Pd/cm<sup>2</sup>, most of the NO desorbs unreacted for the sapphire substrate, as shown in Fig. 2. For Pd/ceria, however, only a small fraction of the NO desorbs intact on both the fresh and reduced surfaces. The TPD curves

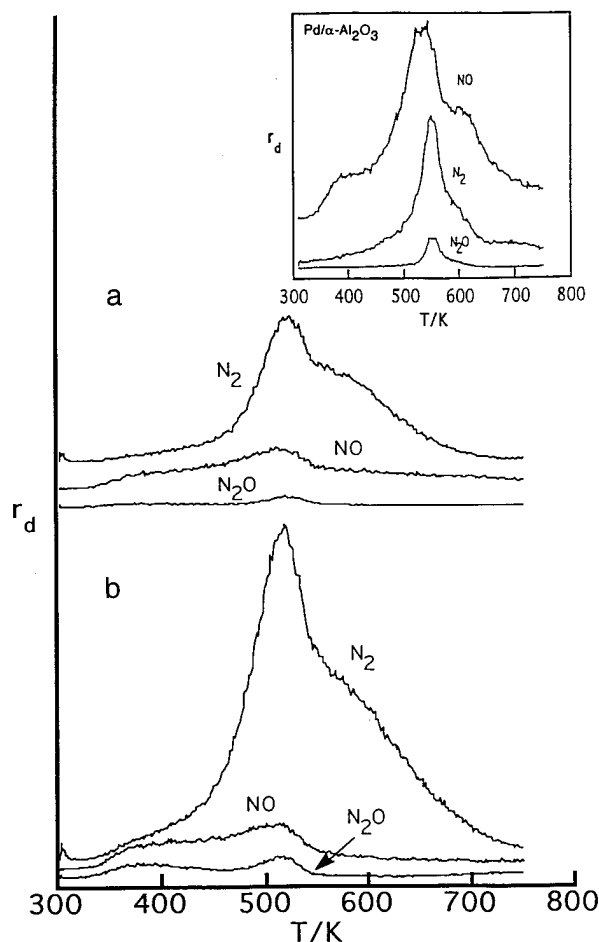


FIG. 2. TPD curves following NO adsorption at room temperature on (a) a fresh and (b) a reduced film of  $5 \times 10^{15}$  Pd/cm<sup>2</sup> on ceria. The NO TPD curves obtained from a Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub> film with the same Pd loading, taken from reference (12), are shown in the insert at the top right of the figure.

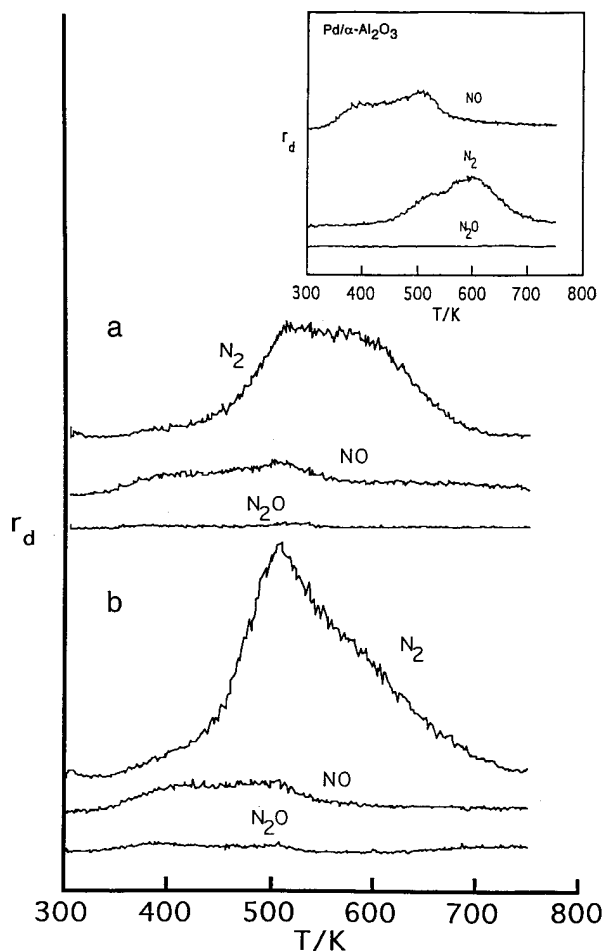


FIG. 3. TPD curves following NO adsorption at room temperature on (a) a fresh and (b) a reduced  $1 \times 10^{15}$  Pd/cm<sup>2</sup> film on ceria. The NO TPD curves obtained from a Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub> film of the same film loading, taken from reference (12), are shown in the insert at the top right of the figure.

on Pd/ceria are qualitatively similar, independent of pretreatment, showing unreacted NO in a peak centered at 510 K, with a leading shoulder extending to 350 K. The main desorption product is N<sub>2</sub>, which desorbs in a narrow feature at 510 K and a second, overlapping, broad feature at ~590 K. A small amount of N<sub>2</sub>O is also observed in peaks at 390 and 510 K. The effect of reducing the Pd/ceria was to dramatically increase the amount of N<sub>2</sub> formed and to increase slightly the N<sub>2</sub>O, while not changing the molecular NO peak. The simultaneous desorption of NO, N<sub>2</sub> and N<sub>2</sub>O at 510 to 550 K on both Pd/ceria and Pd/alumina suggests that some surface processes remain unchanged, but the relative amounts of each product are quite different.

The two important questions are (i) how does reducing the catalyst change the adsorption properties and (ii) how does ceria affect the decomposition of NO. We believe the answer to both these questions is that NO adsorbs on the reduced ceria, which is similar to what was previously re-

ported for lanthana (20). First, we observed negligible adsorption on the ceria without Pd, demonstrating that the oxidized ceria cannot adsorb NO. The evidence that NO can adsorb on the reduced ceria comes from the total amounts of NO which adsorb. A reasonable estimate of the saturation coverages for NO can be obtained by summing the areas under the NO, N<sub>2</sub>, and N<sub>2</sub>O features and comparing these to the saturation CO coverage. For Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001), this ratio was 0.7 (12). On the fresh and reduced Pd/ceria catalysts, these ratios were 0.8 and 3.5, respectively. Obviously, the large amount of NO on the reduced sample suggests that adsorption occurs on the ceria. NO reoxidizes CeO<sub>2-x</sub> and desorbs as N<sub>2</sub>. Adsorption on reduced ceria may also explain why more NO decomposes in TPD on the fresh sample. If Pd is oxidized and ceria reduced, either at room temperature or during the temperature ramp, NO could adsorb on the ceria. Coadsorption of NO and oxygen on Pd should certainly decrease the NO decomposition rate (21) and the CO results suggest that the Pd properties are not significantly changed, so that reaction on reduced ceria is the most reasonable explanation of the increased NO decomposition. The similarities in the desorption temperatures for both fresh and reduced Pd/ceria further agrees with this interpretation.

The TPD curves for  $1 \times 10^{15}$  Pd/cm<sup>2</sup> are qualitatively similar, as shown in Fig. 3. We again find that most of the NO dissociates to desorb as N<sub>2</sub> at the same temperatures observed for the higher Pd coverage, only the amounts are much less. Reducing the catalyst again increases the adsorption uptake. The sum of the peak areas for NO, N<sub>2</sub>, and N<sub>2</sub>O, ratioed to the CO and CO<sub>2</sub> areas, were 1.0 for Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001), 0.9 for fresh Pd/ceria, and 2.0 for reduced Pd/ceria. Since the N<sub>2</sub> desorption features overlap with those observed on Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) at this Pd coverage, desorption from Pd could contribute to the features. We also observe a trace of N<sub>2</sub>O on the Pd/ceria, which was not observed for Pd/sapphire, suggesting that the N<sub>2</sub>O is formed on the oxide.

#### H<sub>2</sub> Adsorption on Pd/CeO<sub>2</sub>

The TPD curves obtained following a saturation exposure of H<sub>2</sub> at 120 K to fresh Pd/ceria catalysts with Pd coverages of  $5 \times 10^{15}$  and  $1 \times 10^{15}$  Pd/cm<sup>2</sup> are given in Fig. 4, along with the corresponding TPD curve for  $5 \times 10^{15}$  Pd/cm<sup>2</sup> on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001). For Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001), one observes a well-defined peak below 200 K for the larger particles, which is attributable to subsurface H<sub>2</sub> (12). This feature is not observed to any great extent on smaller Pd particles on  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001). Surface hydrogen on Pd/ $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) desorbs in a broad feature between 250 and 400 K, essentially independent of particle size. For the Pd/ceria samples, only molecular H<sub>2</sub>, no water, desorbed in two broad peaks at 200 and 320 K. Except for the amount of H<sub>2</sub> which desorbed, both TPD profiles were essentially the same. While H<sub>2</sub> is

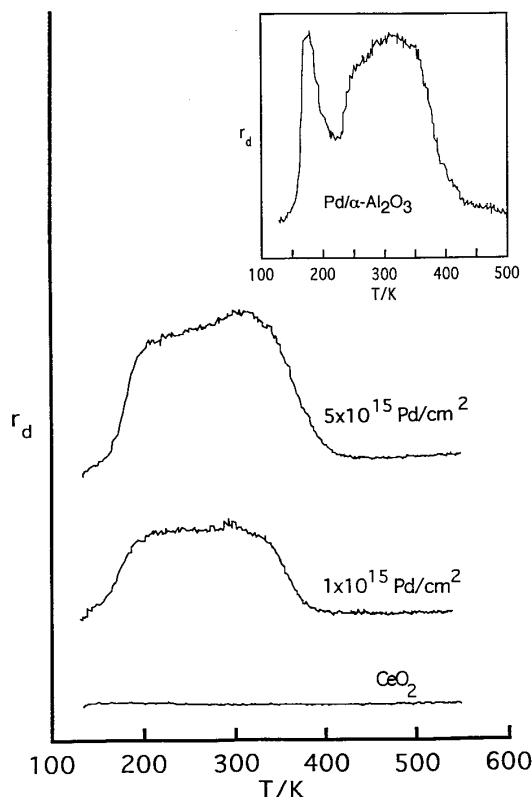


FIG. 4. TPD curves following  $H_2$  adsorption at 120 K on pure ceria as well as for two different loadings of Pd on ceria ( $1$  and  $5 \times 10^{15}$   $Pd/cm^2$ ). The TPD curve obtained from a  $5 \times 10^{15}$   $Pd/cm^2$  loading on  $\alpha-Al_2O_3$ , taken from reference (12), is shown in the insert at the top right of the figure.

seen below 250 K, which might indicate subsurface species, the desorption feature is broad, unlike the alumina case.

The most interesting question regarding  $H_2$  from Pd/ceria is why is water not observed in TPD. If the explanations for CO and NO adsorption on these catalysts are correct, that the Pd is oxidized by contact with the ceria, we should form water from the coadsorbed hydrogen and oxygen. As we discussed earlier, heating the samples in  $1 \times 10^{-7}$  Torr of  $H_2$  for 10 min at 500 K was sufficient to reduce the sample so that adsorption of CO showed only CO in TPD. Therefore, we suggest that water simply readsorbs on the ceria and then either desorbs in a such a broad feature that it is lost in the baseline or is absorbed into the ceria bulk. (The presence of hydrogen in ceria has been discussed by others (28).) The conclusion that water is simply not observed in our TPD measurement was varified in coadsorption measurements with  $O_2$  and  $H_2$ , in which the TPD curves were similar to those reported here and no water was seen.

#### Comparisons with Rh/CeO<sub>2</sub> and Pt/CeO<sub>2</sub>

It is interesting to consider how specific the interactions are between ceria and the catalytic metal. Previously, it was

reported that the properties of Pt and Rh particles on ceria were different in that CO on Rh/ceria resulted in  $CO_2$  formation, while very little  $CO_2$  was observed for Pt/ceria (3, 4). More recently, it was shown that Rh particles on  $CeO_2(111)$  and ceria films annealed at high temperatures do not exhibit  $CO_2$  formation in TPD (22). The pretreatment conditions used for the ceria, therefore, appear to strongly affect the final properties of the catalyst. To do a fair comparison of Pt, Pd, and Rh on ceria, therefore, we examined the desorption of CO from each of the three metals deposited on the same ceria substrate, sputtering the sample clean between the deposition of each metal. The results for fresh Rh/ceria and Pt/ceria, with metal coverages of  $1.5 \times 10^{15}/cm^2$ , are shown in Figs. 5a and 5b.

The results for Rh/ceria are virtually identical to TPD curves reported earlier (3). CO desorbs at 490 K, with a shoulder to lower temperatures, similar to that observed on Rh single crystals. Substantial amounts of  $CO_2$  are also formed, consistent with what would be expected for coadsorbed CO and oxygen. Contrary to previous reports, the results for Pt, Fig. 5b, also show significant  $CO_2$  formation and could be consistent with coadsorbed CO and oxygen. For both Pt and Rh, reduction of the surfaces by heating in either CO or  $H_2$  gave samples which exhibited CO TPD curves similar to that for Pt or Rh on alumina (23), with no evidence for  $CO_2$  formation.

The previous results for Pt/ceria appear to be the result of high-temperature annealing of the ceria, which has

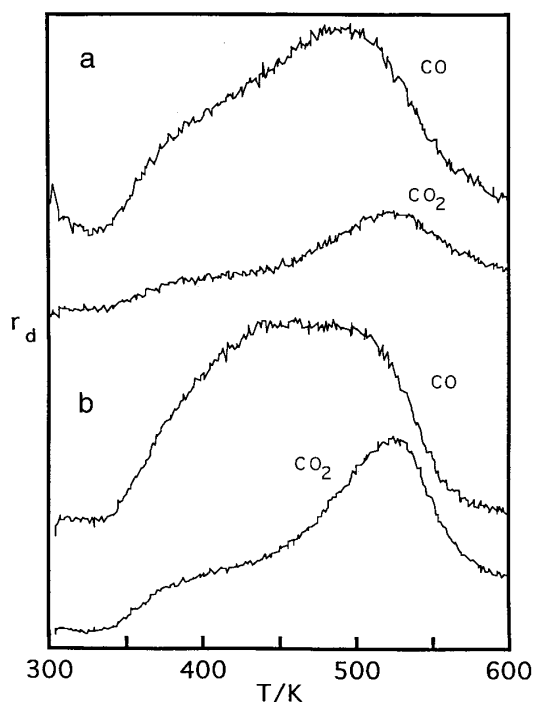


FIG. 5. TPD curves following CO adsorption at room temperature of a fresh film of (a)  $1.5 \times 10^{15}$   $Rh/cm^2$  and (b)  $1.5 \times 10^{15}$   $Pt/cm^2$  on ceria.

already been shown to cause deactivation (5). The NO desorption results reported in this earlier study of Pt/ceria were identical to results for Pt/alumina (24). If it were simply a question of the ceria having been reduced, that study should have observed enhanced N<sub>2</sub> formation and new desorption features, similar to what was observed in the present study on Pd/ceria. This further points out the importance of ceria structure in the adsorption properties of ceria-supported metals.

## DISCUSSION

The central questions addressed in this paper are as follows: (i) What is the nature of support interactions between ceria and group VIII metals? (ii) How do the adsorption and reaction properties of group VIII metals supported on ceria differ from catalysts formed on alumina supports? Each of these issues will be addressed in turn.

First, the ability of CO on Pd, Pt, and Rh to react with lattice oxygen from ceria suggests that all three catalytic metals exhibit similar interactions with ceria. Since each of the metals have different stable oxidation states and form different compounds, interfacial compound formation would not appear to be necessary for the reaction to occur. It is possible that oxidation of CO occurs through a complex at the boundary between the metals and ceria, and evidence for these boundary states has been presented from IR spectra on lanthana-promoted Rh/SiO<sub>2</sub> (25). Since H<sub>2</sub> is equally effective at reducing ceria in our studies, a similar state would have to be invoked for hydrogen. However, it is our opinion that the best explanation for our results is that the metals are oxidized by the reduction of ceria since the TPD curves for CO are so similar to those observed when CO and oxygen are coadsorbed. While the redox process,  $M + \text{CeO}_2 \rightarrow \text{MO}_x + \text{Ce}_2\text{O}_3$ , is not thermodynamically favored for these catalytic metals based on bulk thermodynamic properties (3), there are a number of reasons the thermodynamic data for bulk materials may not be meaningful. First, it is known that CeO<sub>2</sub> can be reduced by as much as 17% without changing from the fluorite structure to the hexagonal Ce<sub>2</sub>O<sub>3</sub> structure (29). Second, the observed sensitivity for CO<sub>2</sub> formation from Rh/ceria on ceria structure suggests that the properties of ceria in these nonannealed films are not the same as for bulk structures (5). Indeed, there is precedence for changes in the free energies of oxides like ceria with particle size in that high-pressure forms of ZrO<sub>2</sub> and Y<sub>2</sub>O<sub>3</sub> can be stabilized at low pressures by forming small crystallites (26).

Electronic effects are often invoked to explain support effects, but these do not appear to be important for ceria. Following reduction of the ceria, which should maximize interactions based on most theories of support interactions, the desorption curves for CO from Pd/ceria are identical to those found for Pd on an inert substrate,  $\alpha$ -Al<sub>2</sub>O<sub>3</sub>(0001) (12). Similar results were found for Rh and Pt. Since desorp-

tion temperatures are a sensitive measure of the adsorption properties of the catalyst, changes in the metal properties should be reflected in the TPD curves. There is also no evidence for ceria migration onto the metals, such as has been reported for titania-supported metals (27).

The picture of ceria support effects that emerges, then, is one in which oxygen and possibly NO move relatively freely between the ceria and the catalytic metal. Lattice oxygen from CeO<sub>2</sub> at the metal-ceria boundary provides oxygen to the metal for oxidation reactions, while reduced sites at the boundary provide adsorption sites for NO. These reduced sites can be oxidized by NO, giving up N<sub>2</sub> and completing the oxidation-reduction cycle.

Regarding the adsorption and reaction properties of ceria-supported Pd, the TPD results show that there are significant changes due to the presence of ceria. For CO, obviously, the reaction with lattice oxygen from the ceria provides a second pathway for CO oxidation. Previous work with Rh/ceria has shown that this second pathway exhibits different reaction orders for both CO and O<sub>2</sub> from that observed for Rh/alumina under reducing conditions and also exhibits a lower activation energy (18). Therefore, the oxidation process observed in TPD influences the steady-state reaction rates, at least under some conditions. The results reported here for NO suggest that reactions of this molecule will also be strongly affected by the presence of ceria under net reducing conditions. The relatively free movement of molecules between sites on the catalytic metal and on the ceria provides a means for enhancing NO dissociation. This could be very important for metals like Pt and Pd which are not active for NO dissociation. Therefore, based on our TPD results, one would predict that the presence of ceria could significantly enhance NO reduction. Comparisons of rates for NO reduction by CO on Pd/alumina and Pd/ceria are presently being performed in our laboratory to test this prediction.

## SUMMARY

The desorption measurements in this study indicate that the effect of ceria on Pd is very similar to that found for Rh and Pt. There is no evidence for electronic interactions which modify the adsorption properties of the metal, but it appears that lattice oxygen from the ceria can be transferred to the metal surface. This results in CO<sub>2</sub> formation at relatively low temperatures upon the adsorption of CO. The reduction of ceria by oxygen transfer also frees sites for NO adsorption, and NO decomposes readily on reduced ceria. This may provide an additional reaction pathway for NO decomposition.

## ACKNOWLEDGMENTS

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